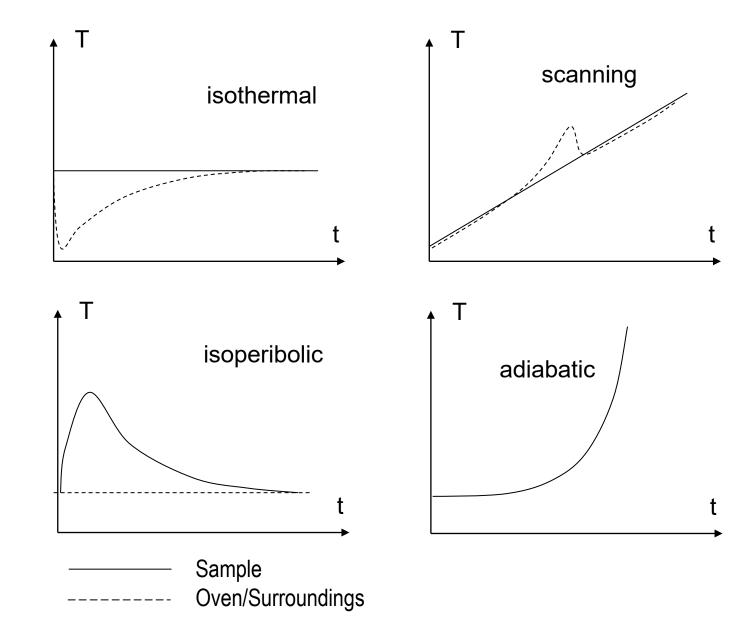
Calorimetry and Thermal Analyses Applications in Process Safety

Module 3

ENG 431: Safety of chemical Processes

Annik Nanchen

Temperature programme (mode of operation)



Adiabacity Factor

Φ-Factor

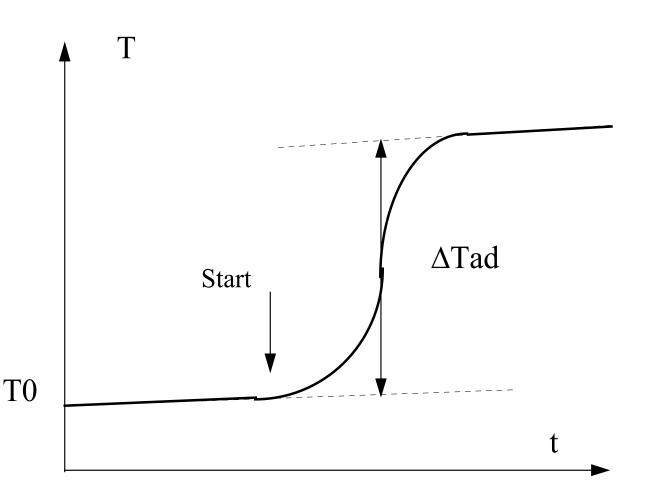
- Thermal Inertia of the System/Apparatus
- Part of the reaction heat is used to heat up the calorimetric cell

$$\Phi = \frac{M_r \cdot c_{p,r}' + M_{cell} \cdot c_{p,cell}'}{M_r \cdot c_{p,r}'} = 1 + \frac{M_{cell} \cdot c_{p,cell}'}{M_r \cdot c_{p,r}'}$$

- A perfectly adiabatic system has a Φ factor of 1
- M_{cell} large $\rightarrow \Phi$ factor increases

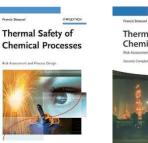
Correction for $\Phi > 1$

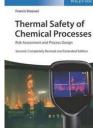
$$\Delta T_{ad} = \Phi \cdot \Delta T_{mes} \quad T_f = T_0 + \Phi \cdot \Delta T_{mes}$$

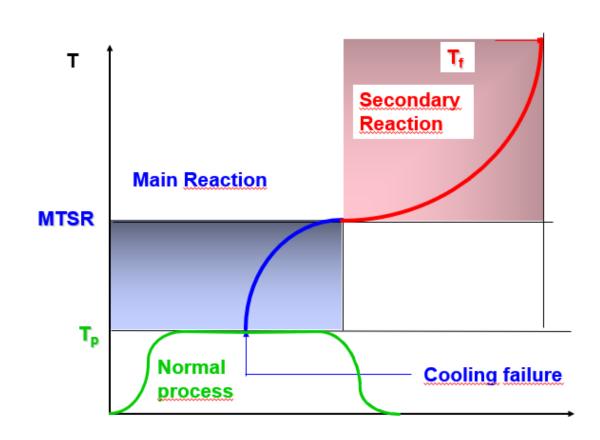


What calorimetric measurements are used to assess the cooling failure scenario?

- Main reaction
 - Mainly Reaction Calorimetry
 - Screening: micro-calorimetry
- Secondary reaction
 - Micro-calorimetry
 - Adiabatic measurements
 - High sensitivity calorimetry
- Both
 - Adiabatic measurements
 - Micro-calorimetry



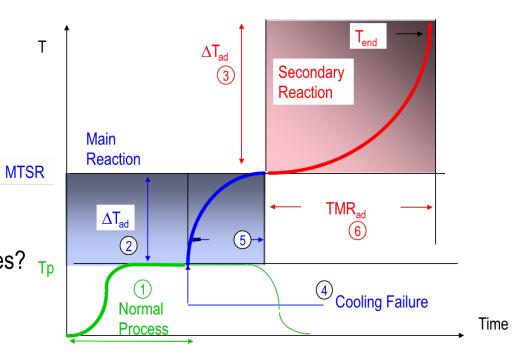




Chapter 4

Synthesis Reaction - Data

- Heat release rate under normal process conditions
 - Question 1: is there enough cooling capacity for isothermal conditions?
- Reaction Energy
 - Thermal Potential/Consequences
 - Question 2: how high is the MTSR (maximum temperature of the synthesis reaction)?
- Accumulation
 - Thermal Potential/Consequences
 - Question 2: how high is the MTSR (maximum temperature of the synthesis reaction)?
 - Question 4: when does the cooling failure have the worst consequences? $_{\mathsf{Tp}}$
- Reaction calorimetry to get heat release rate, reaction energy and accumulation
 - RC1, CPA
- Screening methods will only provide the reaction energy
 - DSC, C80



• Reproduce the reaction as done/foreseen at industrial scale





Principles

- Heat Balance
 - Balance on the heat carrier in the jacket

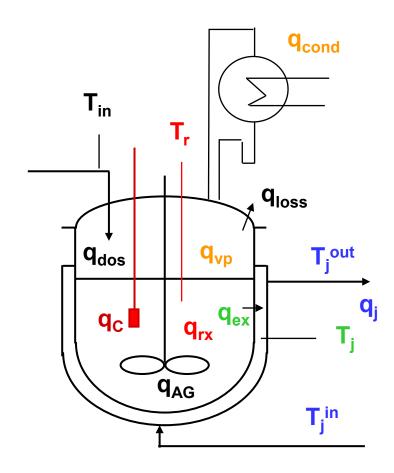
$$q_{j} = \dot{m} \cdot Cp' \cdot \left(T_{j,out} - T_{j,in}\right)$$

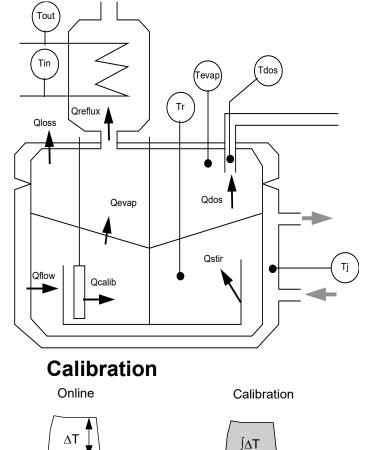
- Heat flow
 - Measuring the heat flow exchanged with the jacket

$$q_{EX} = U \cdot A \cdot \left(T_j - T_R\right)$$

- Compensation
 - Measuring the power of an electrical heater maintaining the temperature at set point with surplus cooling

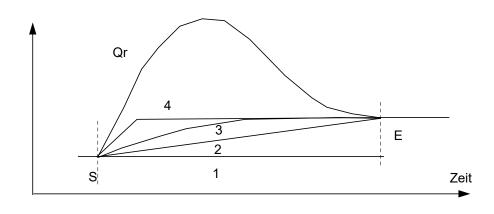
$$q_{RX}$$
 linked to q_c



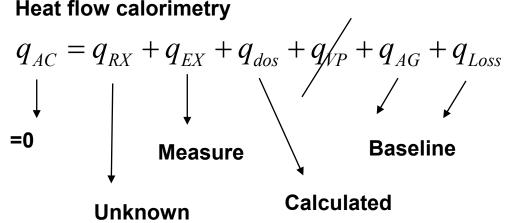


∫Qc

Baseline



Heat flow calorimetry



- Preparative scale (100 ml to 2 L)
- Stirred tank reactor
- Controlled feed of reactant
- Distillation
- Mimics industrial processes
- Physical similarity
- Scale up data





RC1 Reaction Calorimeter

RC1-Calorimeter, Mettler-Toledo:

• T: -20 – 200°C

• P: 0 – 50 bar

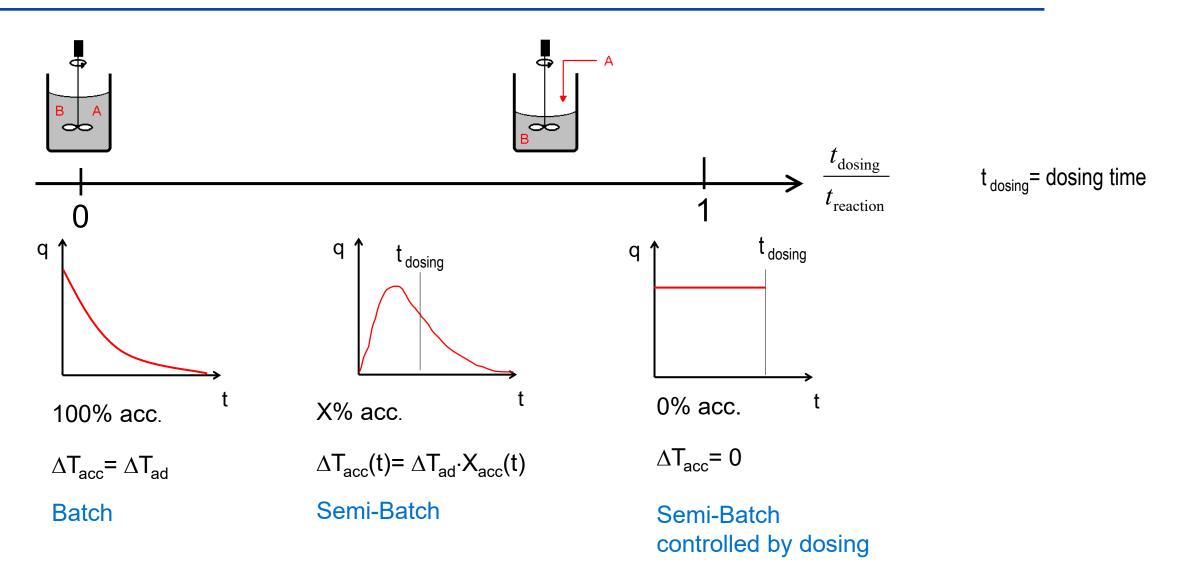
• V: 200 – 800 ml







Dosing of Reagents – Batch - Semi-Batch:

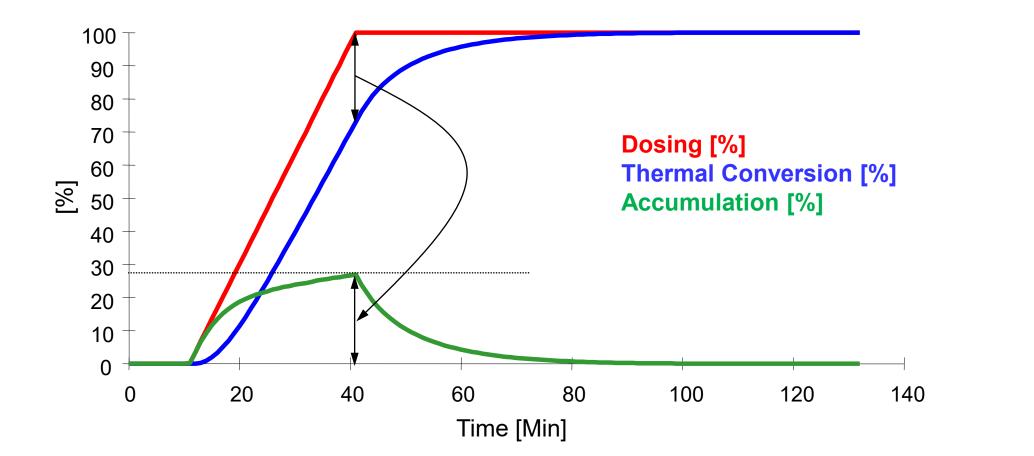


• ΔT_{acc} is the temperature increase that has to be considered when calculating the MTSR

Given by the measurement (known) Derived from measured data

Parameter of interest

Accumulation [%] = Dosing [%] – thermal Conversion [%]



Chemisens CPA 202

Heat Flow Calorimeter

- Uses a Peltier array for heating and cooling rather than jacketed vessel
- Uses a heat flow sensor which measures power directly

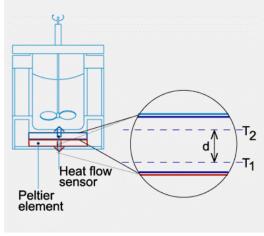
Advantages

- Calibrations not required on individual tests
- Small volume 30-180 ml

Disadvantages

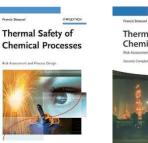
- Solids charging difficult
- Difficult to see inside vessel
- No bottom run

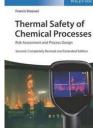


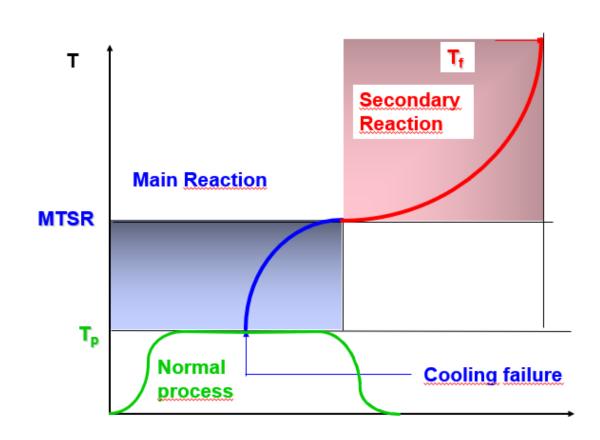


What calorimetric measurements are used to assess the cooling failure scenario?

- Main reaction
 - Mainly Reaction Calorimetry
 - Screening: micro-calorimetry
- Secondary reaction
 - Micro-calorimetry
 - Adiabatic measurements
 - High sensitivity calorimetry
- Both
 - Adiabatic measurements
 - Micro-calorimetry



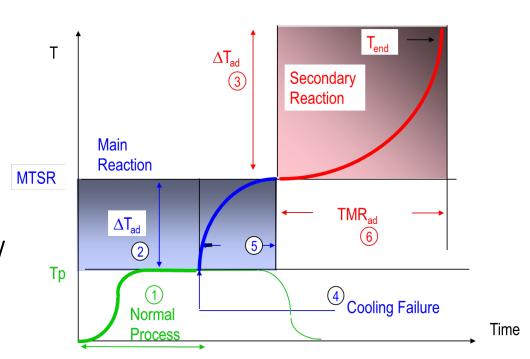


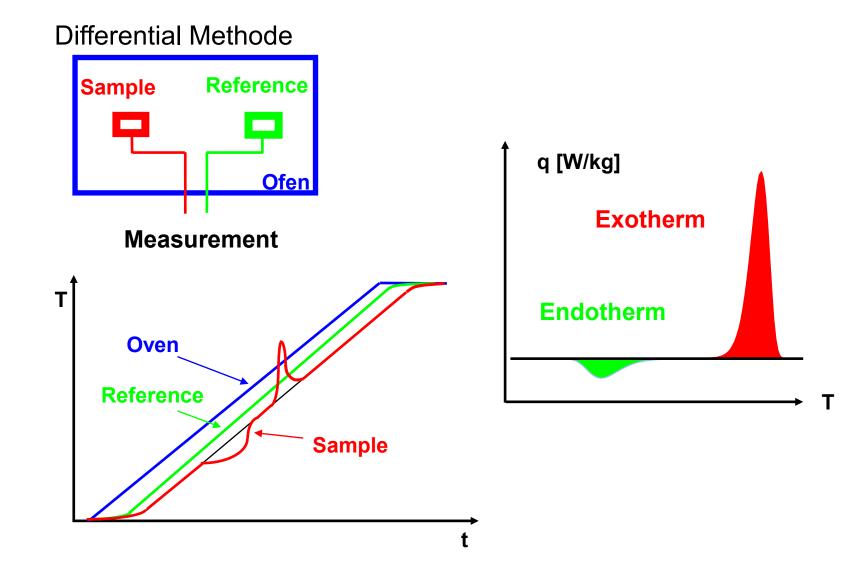


Chapter 4

Secondary reaction- Data

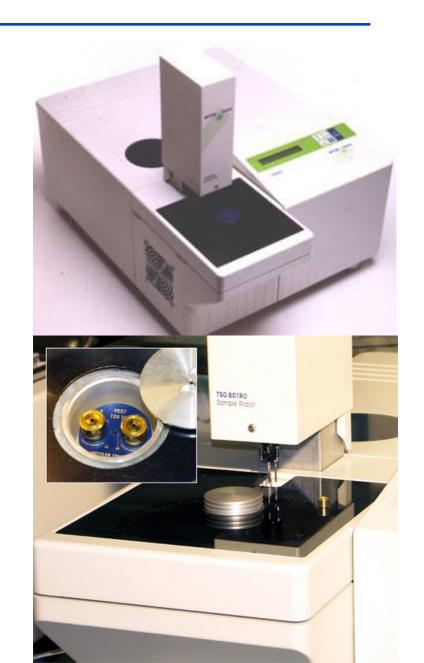
- Reaction/Decomposition Energy
 - Thermal Potential/Consequences
 - question 3 cooling failure scenario: how high is the final temperature?
- TMRad (or tmr_{ad})
 - Probability of triggering the decomposition
 - question 6 cooling failure scenario: how long does it take from the MTSR to the final T?
- Micro-calorimetry will provide the reaction/decomposition energy and will be used to determine q' as a function of T (to calculate TMRad)
 - DSC, C80
- Adiabatic measurements :TMRad at one T and decomposition/reaction energy
 - ARC, Dewar





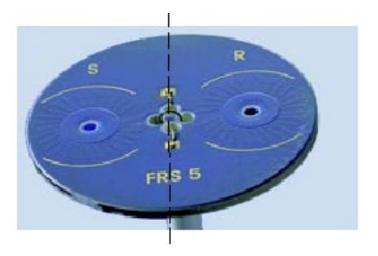
- « Micro scale »
 - Amount mg
 - Safe, even with highly exothermic samples
 - Mostly used to study decompositions (stability)
- Quantitative Measurement
 - Energy and power
 - Large T-range
- Short Cycle times → used for screening
 - Process deviations / route selection
 - Catalytic effects
 - Solvent effects
- Mode:
 - Isothermal
 - Scan (typically 4°C/min from 30 to 400°C)

Practical Sensitivity: ~ 20W/kg

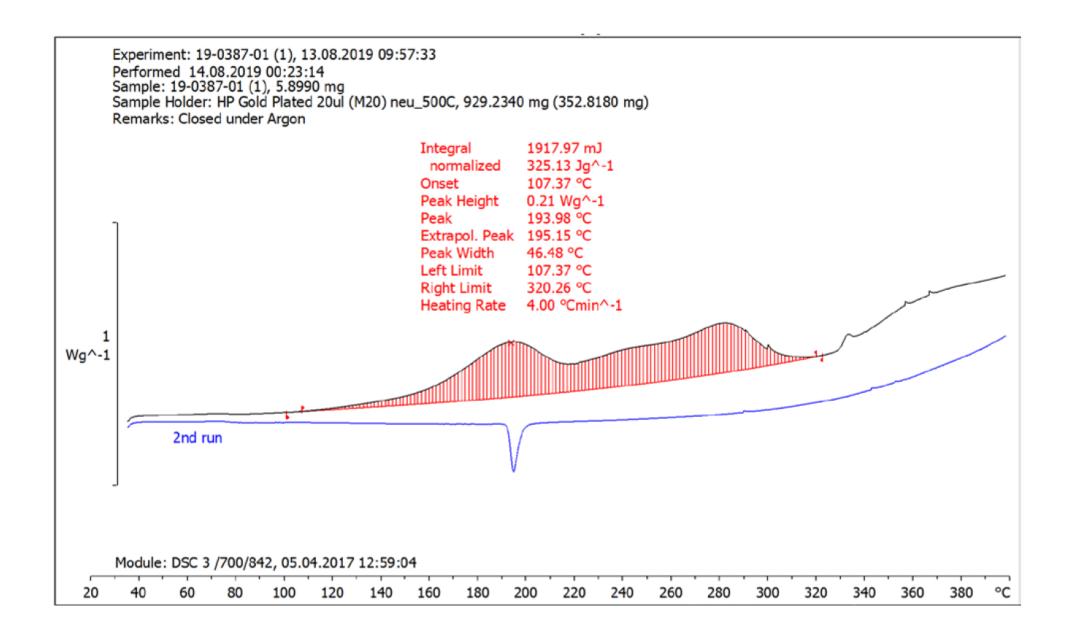


DSC for safety studies

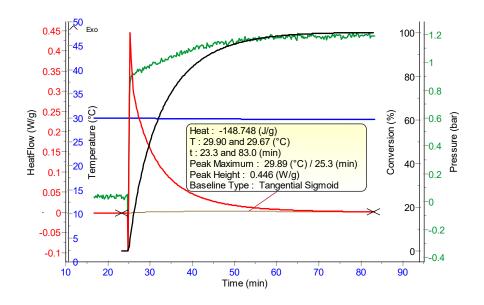
- Robust and sensitive sensor head
- Pressure resistant tight crucibles
 - No evaporation
 - No product loss
 - No catalytic effects
- Thermal finger print of a reactive system
- Determination of energy release by reaction(s)
- Working under controlled atmosphere is possible







Tian-Calvet Calorimeter (C80)

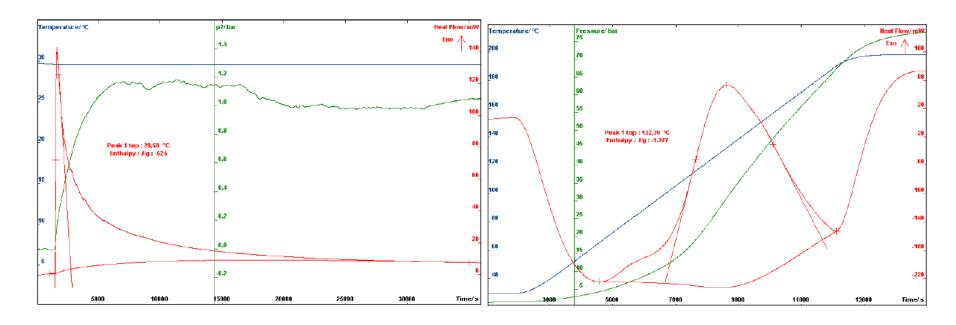


- T: -100 300°C (max. 1°C/min.)
- P: 0 200 bar
- V: 100 mg 1 g
- Small scale reaction calorimetry
- Options: mixing, gas reactions, pressure measurement
- Mixing cell: combined measurement of synthesis and decomposition reaction (thermal stability)
- Practical Sensitivity (screening): ~ 2W/kg



Reaction in a Calvet calorimeter

• Setaram C80



Process under isothermal conditions

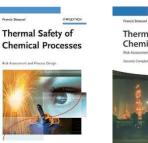
Thermal stability of final reaction mass

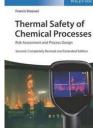
Micro-calorimetry to determine reaction energy

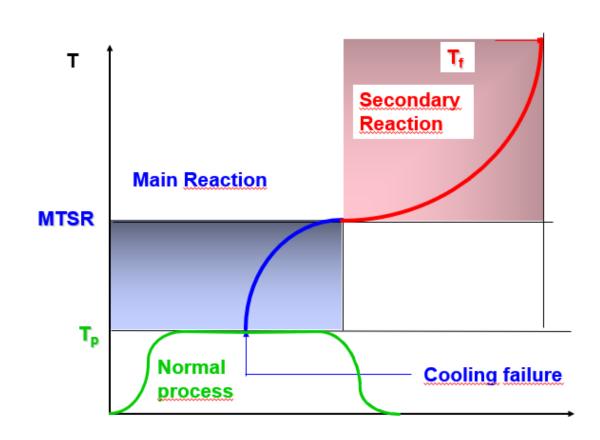
- Mix the reactant (cold mixture) and perform a dynamic measurement
 - Reaction energy
 - Decomposition energy
- Advantages
 - Small scale
 - Screening
- Disadvantages
 - No mixing
 - No information on heat release rate, accumulation
 - Does the reaction run to completion?

What calorimetric measurements are used to assess the cooling failure scenario?

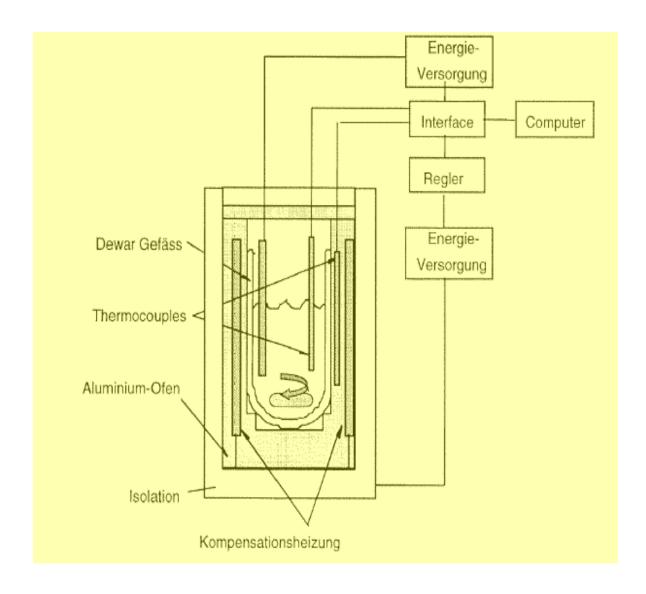
- Main reaction
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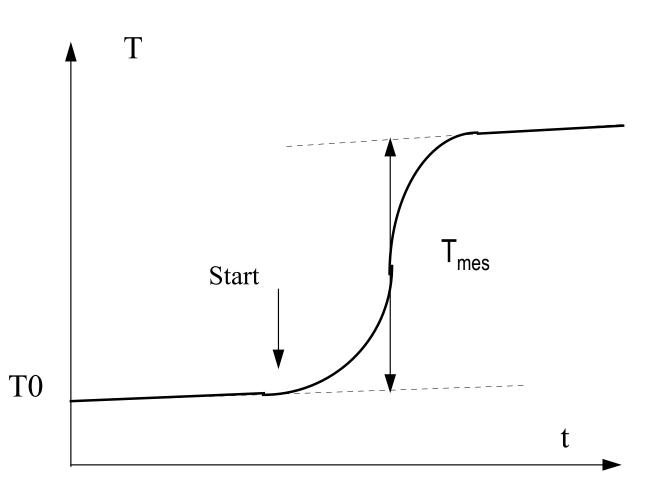
Chapter 4



- 300-800 ml
- Thermos flask with vacuum jacket to minimize heat losses
- Different materials (e.g. glass, stainless steel)
- With closure or open
- Stirrer, connections for addition of liquids, sampling, pressure and temperature sensors etc.
- Adiabatic tests performed in temperature controlled oven
- Hazards for the operator (destruction of oven/Dewar)

Dewar

- Measure a temperature increase
- Is this the adiabatic temperature increase?
 - Depends on the heat losses and on the energy required to heat the Dewar
 - → adiabacity factor: **Φ** factor



Adiabacity Factor

Φ-Factor

- Thermal Inertia of the System/Apparatus
- Part of the reaction heat is used to heat up the calorimetric cell

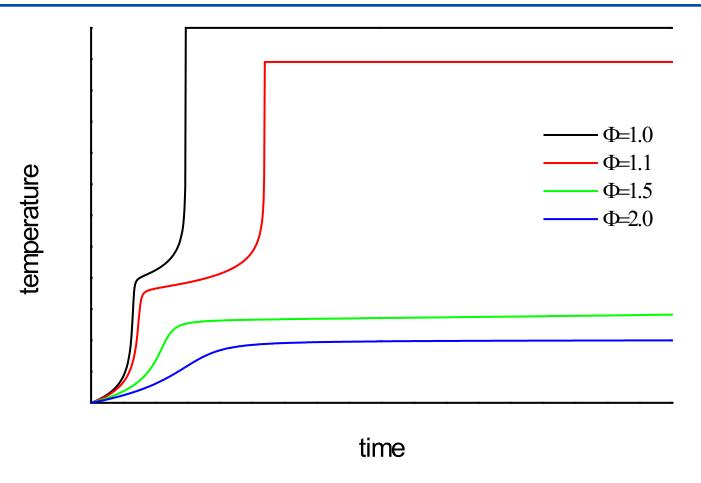
$$\Phi = \frac{M_r \cdot c'_{p,r} + M_{cell} \cdot c'_{p,cell}}{M_r \cdot c'_{p,r}} = 1 + \frac{M_{cell} \cdot c'_{p,cell}}{M_r \cdot c'_{p,r}}$$

- A perfectly adiabatic system has a Φ factor of 1
- $-M_{cell}$ large $\rightarrow \Phi$ factor increases

Correction for $\Phi > 1$

$$\Delta T_{ad} = \Phi \cdot \Delta T_{mes}$$

$$T_f = T_0 + \Phi \cdot \Delta T_{mes}$$



Conclusions

- Data must be corrected for Φ
- Need to measure at higher T

- Which is the plant situation?
- Which curve is the measured one?

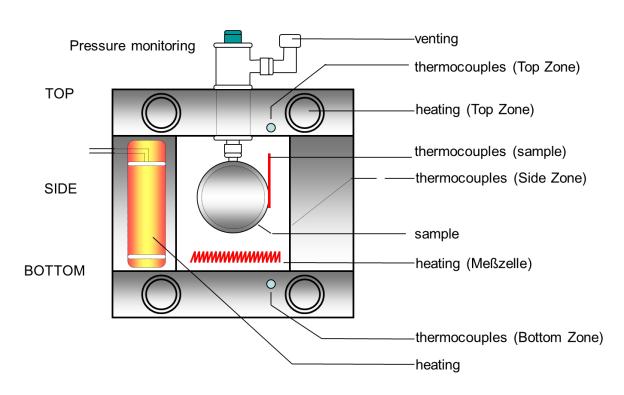
Observations from the figure

- The temperature rise is larger in the plant than in the test
- The time taken for the runaway reaction is shorter in the plant
- The rates of temperature and pressure rise are higher in the plant
- Runaway not measured at Φ 1.5 and 2.0

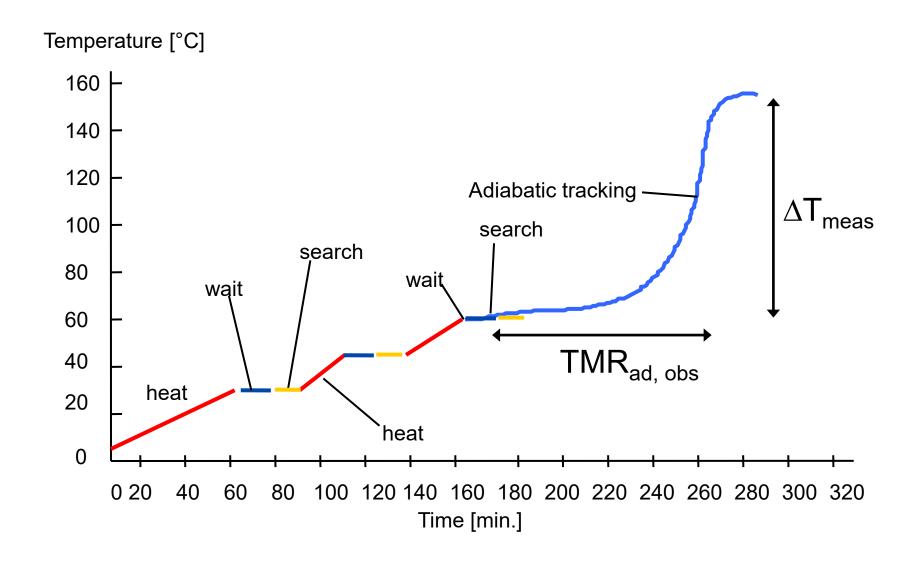
Accelerating Rate Calorimeter (ARC)

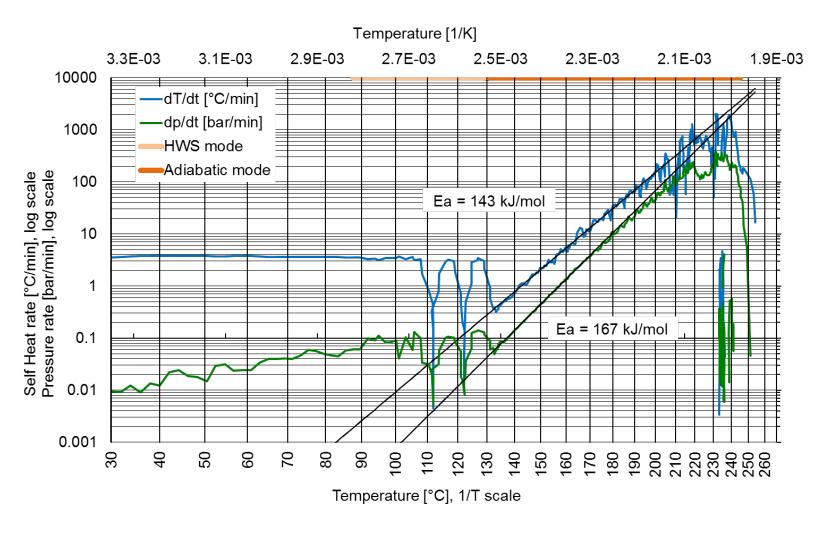
- T: 30 500°C
- P: 0 170 bar
- V: 4 50 ml
- Different test bomb material (HC, Ti)
- Different modes of operation (adiabatic tracking; heat-wait-search)











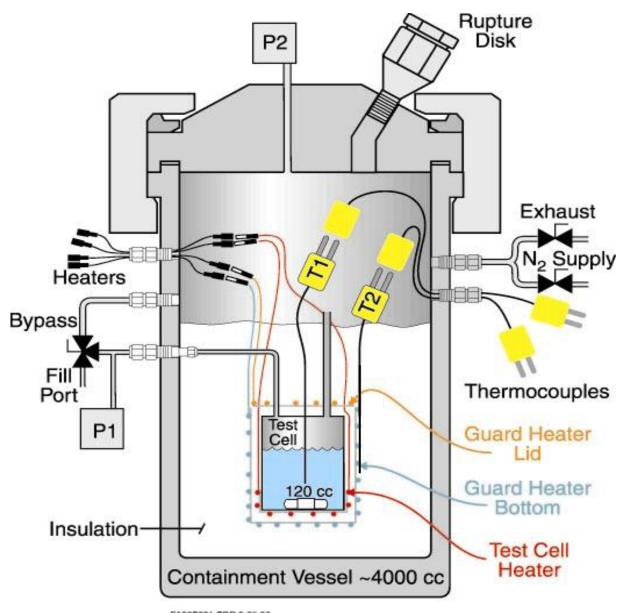
Temperature and pressure rate

Vent Sizing Package 2



- T: 30 500°C (tracking up to 300°C/min.)
- P: 0 130 bar (tracking up to 650 bar/min)
- V: 50 100 ml
- Typical Phi-factor: 1.1
- Gas and Liquid Dosing, Sampling, Stirring
- Different modes of operation (e.g. Closed or Open System, Relief Valve simulation, Depressurization/Blowdown tests, Quench reactions)

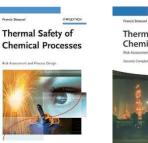


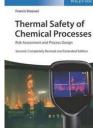


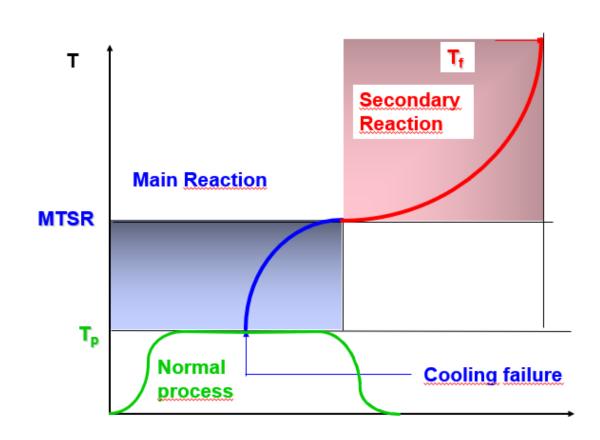
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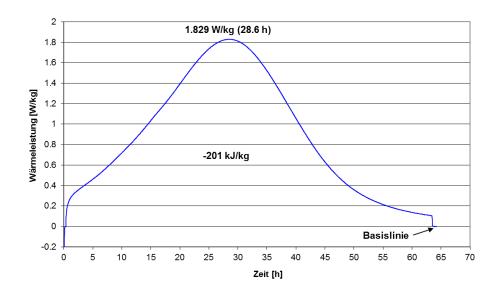




Chapter 4

TAM Thermal Activity Monitor



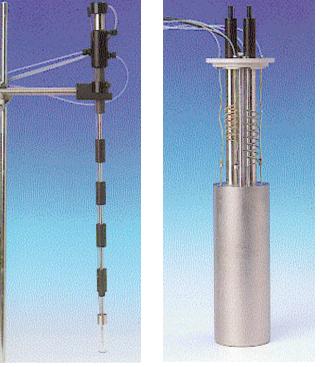


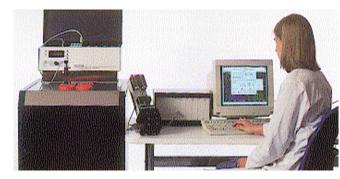
- T: isotherm at 30 150°C
- V: 1-4 ml
- Very high sensitivity (0.01 W/kg)
- Measurement under defined gas atmosphere (e.g. N₂, air)

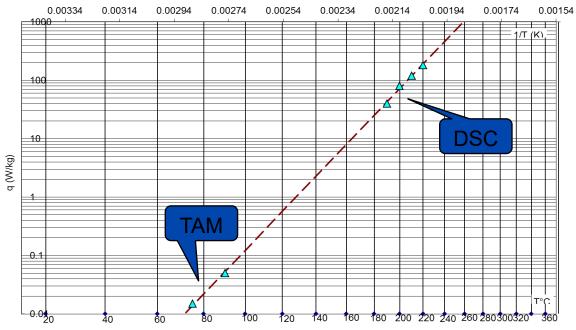
TAM Thermal Activity Monitor

Stability assessment for storage or transportation

Detection of very low heat generation rates

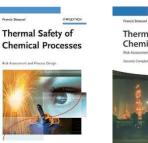


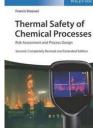


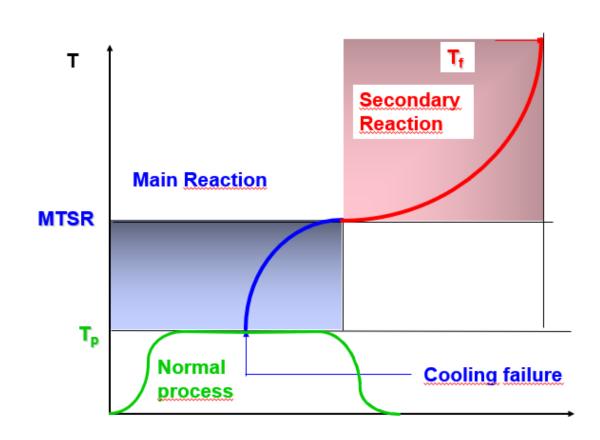


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 - Micro-calorimetry
 - Adiabatic measurements
 - High sensitivity calorimetry
- Both
 - Adiabatic measurements
 - Micro-calorimetry







Chapter 4

Measuring both synthesis reaction and decomposition

- Micro-calorimetry: only energy information for the main reaction and no mixing
- Adiabatic measurements:
 - Careful with phi factor
 - Data for one starting temperature
- Ideally: combination of measurements
 - Reaction calorimetry for main reaction
 - Micro-calorimetry for decomposition reaction
 - Adiabatic measurements to confirm or to look at specific situations
- High sensitive measurements (TAM) when assessing storage, transport (avoiding large extrapolation of data)

Comparison

Method	Measuring principles	Application field	Sample size	Temperature range	Sensitivity (W kg ⁻¹) ^{a)}
Differential scanning calorimetry (DSC)	Differential, ideal flux, or isoperibolic	Screening and secondary reactions	1–50 mg	−50 to 500°C	2 ^{b)} -10
Calvet C80 (BT 2.15)	Differential, ideal flux	Main and secondary reactions	0.1-3 g	30-300 °C (-196 to 200 °C)	0.1-1 ^{c)}
Accelerating rate calorimeter (ARC)	Ideal accumulation	Secondary reactions	0.5–3 g	30-400°C	0.5
Vent Sizing Package (VSP)	Ideal accumulation	Main and secondary reactions	50-100 g	30-350°C	0.2
Sensitive detector of exothermal processes (SEDEX)	Isoperibolic, adiabatic	Secondary reactions, storage stability	2-100 g	0-400°C	0.5 ^{d)}
RADEX	Isoperibolic	Screening, secondary reactions	1.5–3 g	20-400°C	2
SIKAREX	Ideal accumulation, isoperibolic	Secondary reactions	5-50 g	20-400°C	0.25
Reaction calorimeter	Ideal flux or heat balance	Main reactions	50-2000 g	−40 to 250 °C	1.0
Thermal activity monitor (TAM)	Differential, ideal flux	Secondary reactions, storage stability	0.5–3 g	30-150°C	0.01
Dewar	Ideal accumulation	Main reactions and thermal stability	100-1000 g	30-250°C	e)

a) Typical values.

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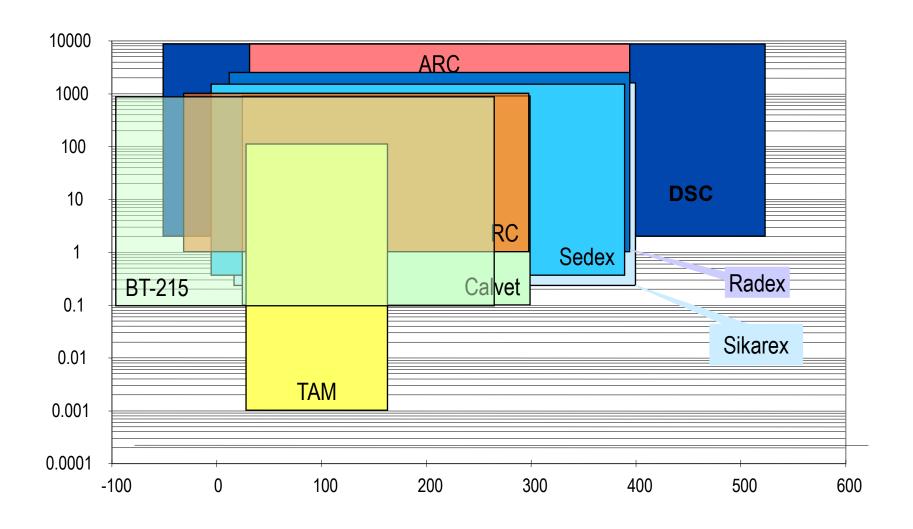
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b) Most recent instruments under optimal conditions.

c) Depending on the sample mass.

d) Depends on cell used.

e) Depends on volume and Dewar quality.



Summary

- Study of main reaction:
 - Reaction calorimeters (RC1, CPA)
 - Data obtained: Reaction energy Q'_{rxn} , heat release rate q'_{rxn} , accumulation $X_{acc} \rightarrow can calculate MTSR$
 - Screening possible in DSC and C80
- Study of decomposition reactions
 - Screening: DSC, C80, ARC (adiabatic)
 - Data obtained DSC and C80 from scan experiment:
 - decomposition energy, information on gas production (C80).
 - TMRad is calculated (see lecture on thermal stability)
 - Data obtained for ARC
 - TMRad and ∧Tad
 - Correction for non adiabacity (Φ factor)
 - Low heat release rate (e.g. Storage, Transport)
 - TAM; isothermal measurement
 - Data obtained: decomposition energy, heat release rate
 - TMRad calculated (see lecture on thermal stability), or heat balance calculated (see lecture on heat confinement)
 - Adiabatic: VSP, Dewar
 - Data obtained: TMRad and ∆Tad
 - Correction for non adiabacity (Φ factor)